

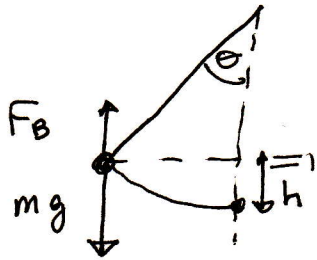
Problem 1

pendulum frequency in air:  $\omega = \sqrt{\frac{g}{l}} = 2\pi f \Rightarrow$

$$\Rightarrow l = \frac{g}{4\pi^2 f^2} = \frac{9.8}{4\pi^2} \text{ m} = 0.248 \text{ m} \Rightarrow \boxed{l = 24.8 \text{ cm}}$$

length of string

In water, there is buoyant force:



$$F_B = \rho_w \cdot V \cdot g, \quad V = \text{volume of ball}$$

$$F_B = \frac{\rho_w}{\rho_{\text{ball}}} \cdot mg, \quad \rho_{\text{ball}} = \frac{m}{V} = \frac{11}{4} \frac{\text{g}}{\text{m}^3} = 2.75 \text{ g/cm}^3$$

so net force is  $F = mg - F_B = mg \left(1 - \frac{\rho_w}{\rho_{\text{ball}}}\right)$

So  $g$  is reduced by the factor  $1 - \frac{\rho_w}{\rho_{\text{ball}}} = 1 - \frac{1}{2.75} = 0.636$

So the frequency is reduced by factor  $\sqrt{0.636} = 0.798 \approx 0.8$

$$\Rightarrow \boxed{f = 0.8 \text{ Hz in water}} \quad (a)$$

(b) In damped oscillation,  $\omega' = \sqrt{\omega^2 - \gamma^2}$ , and  $\Theta(t) = A e^{-\gamma t} \cos \omega' t$

In critical damping,  $\boxed{\gamma = \omega = 2\pi f = 5.01 \text{ s}^{-1}}$

In  $\Theta$  to go from  $10^\circ$  to  $0.1^\circ \Rightarrow e^{\gamma t} = 100 \Rightarrow t = \frac{\ln 100}{\gamma} \Rightarrow$

$$\Rightarrow \boxed{t = 0.92 \text{ s}}$$

(c) The initial energy is  $E_{\text{in}} = mgh \times 0.636$

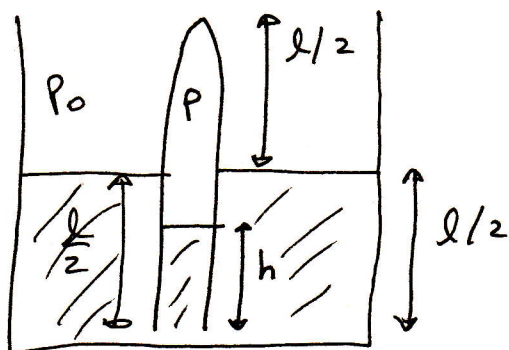
$$h = l - l \cos \theta = 0.38 \text{ cm} \Rightarrow E_{\text{in}} = 11 \times 10^{-3} \times 9.8 \times 0.636 \times 0.38 \text{ J} = 0.026 \text{ J}$$

final energy  $\sim 0 \Rightarrow E_{\text{in}}$  gets transformed into heat

$$\boxed{\Delta S = \frac{E_{\text{in}}}{T} = \frac{0.026 \text{ J}}{393 \text{ K}} = 6.6 \times 10^{-5} \frac{\text{J}}{\text{K}}}$$

## Problem 2

$P_0 = 101,300 \text{ N/m}^2$  is atmospheric pressure



The gas in the tube occupies a <sup>smaller</sup> ~~larger~~ volume than initially  $\Rightarrow$  has higher pressure.

$$PV = \text{constant} \Rightarrow P(l-h) = P_0 l \Rightarrow \boxed{P = P_0 \frac{l}{l-h}}$$

equating pressure at the tube opening:

$$P_0 + \rho g \frac{l}{2} = P + \rho g h = \frac{P_0 l}{l-h} + \rho g h \Rightarrow$$

$$\Rightarrow \frac{P_0}{\rho g} + \frac{l}{2} = \frac{P_0}{\rho g} \frac{l}{l-h} + h \Rightarrow \frac{P_0}{\rho g} (l-h) + \frac{l^2}{2} - \frac{lh}{2} = \frac{P_0 l + hl - h^2}{\rho g}$$

$$\Rightarrow \cancel{\frac{P_0}{\rho g} l} - \frac{P_0}{\rho g} h + \frac{l^2}{2} - \frac{lh}{2} = \cancel{\frac{P_0}{\rho g} l} + lh - h^2 \Rightarrow$$

$$= h^2 - h \left( \frac{3}{2} l + \frac{P_0}{\rho g} \right) + \frac{l^2}{2} = 0$$

$$\frac{P_0}{\rho g} = \frac{101,300}{13.6 \times 1000 \times 9.8} \text{ m} = 0.76 \text{ m} = 76 \text{ cm} \Rightarrow \text{with } l = 80 \text{ cm}$$

$$\frac{3}{2} l + \frac{P_0}{\rho g} = 196 \text{ cm}, \quad \frac{l^2}{2} = 3200 \text{ cm}^2$$

$$h^2 - 196 h + 3200 = 0 \Rightarrow$$

$$h = \left( \frac{196}{2} \pm \sqrt{\left( \frac{196}{2} \right)^2 - 3200} \right) \text{ cm} = (98 \pm 80) \text{ cm} \Rightarrow \boxed{h = 18 \text{ cm}}$$

### Problem 3

Speed of sound  $u = \sqrt{\frac{B}{\rho}}$ ,  $B = -V \frac{dP}{dV}$

$\rho = \frac{\text{mass}}{\text{volume}} = \frac{nM}{V}$ , with  $M = \text{molecular mass} = \frac{4g}{\text{mol}}$  for He

Isothermic:  $P = \frac{nRT}{V}$ ,  $\frac{dP}{dV} = -\frac{nRT}{V^2} \Rightarrow B = \frac{nRT}{V} \Rightarrow$

$\Rightarrow \frac{B}{\rho} = \frac{nRT \cdot V}{V \cdot nM} = \frac{RT}{M} = \frac{8.314 \text{ J K}^{-1} \text{ mol}^{-1} \times 273 \text{ K}}{4 \times 10^{-3} \text{ kg mol}^{-1}} =$

$= 567,430.5 \frac{\text{m}^2}{\text{s}^2} \Rightarrow \boxed{u = 753.3 \text{ m/s}} \quad (a)$

(b)  $PV^\gamma = \text{const} \Rightarrow P = \frac{\text{const}}{V^\gamma} \Rightarrow \frac{dP}{dV} = -\frac{\gamma \text{const}}{V^{\gamma+1}} = -\frac{\gamma P}{V} \Rightarrow$

$\Rightarrow B = \gamma P = \frac{\gamma nRT}{V} \Rightarrow \text{same as before except for } \gamma \text{ factor.}$

$\gamma = \frac{5}{3}$  for ideal gas  $\Rightarrow$

$\boxed{u = \sqrt{\frac{5}{3}} \times 753.3 \frac{\text{m}}{\text{s}} = 972.5 \text{ m/s}}$

(c) Write  $T = 273 + t$ , with  $t$  the temperature in  $^\circ\text{C}$

$u = \sqrt{\frac{\gamma R (273+t)}{M}} = \sqrt{\frac{\gamma R \cdot 273}{M}} \sqrt{1 + \frac{t}{273}} \approx \sqrt{\frac{\gamma R \cdot 273}{M}} \left(1 + \frac{t}{2 \cdot 273}\right) =$

$= 972.5 \left(1 + \frac{t}{546}\right) \frac{\text{m}}{\text{s}} = \boxed{(972.5 + 1.78 t) \frac{\text{m}}{\text{s}}}$

$\Rightarrow \boxed{b = 1.78}$

### Problem 4

The instrument plays at frequency  $f$ . The frequency heard by G from the guitar in the moving car is

$$f' = \frac{1}{1 - \frac{v_c}{v_s}} f, \text{ with } v_c = \text{speed of car. Hence}$$

$$f' - f = \left(1 - \frac{1}{1 - \frac{v_c}{v_s}}\right) f = \frac{v_c/v_s}{1 - v_c/v_s} f \Rightarrow$$

$$f = \frac{1 - v_c/v_s}{v_c/v_s} (f' - f). \text{ With } f' - f = 25 \text{ Hz} \Rightarrow \boxed{f = 403.75 \text{ Hz}}$$

The frequency heard by M from the guitar on the ground is

$$f' = \left(1 + \frac{v_c}{v_s}\right) f \Rightarrow f' - f = \frac{v_c}{v_s} f = 23.54 \text{ Hz}$$

So M hears 23.54 beats/s

(b)  $\lambda f = v = \sqrt{\frac{F_T}{\mu}} = \sqrt{\frac{F_T \cdot l}{m}}$ , fundamental is  $\lambda = 2l \Rightarrow$

$$\Rightarrow 2lf = \sqrt{\frac{F_T l}{m}} \Rightarrow 4l^2 f^2 = \frac{F_T l}{m} \Rightarrow l = \frac{F_T}{4m f^2}$$

$$\Rightarrow l = \frac{100}{4 \cdot 0.5 \times 10^{-3} \times 403.75^2} \text{ m} = 0.307 \text{ m} \Rightarrow \boxed{l = 30.7 \text{ cm}}$$

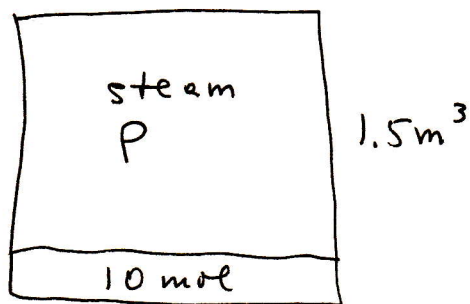
(c) Wavelength of fundamental string vibration

$$\boxed{\lambda = 2l = 61.34 \text{ cm}}$$

Wavelength of sound wave:

$$\lambda_s = \frac{v_s}{f} = \frac{343 \text{ m/s}}{403.75/\text{s}} = 0.85 \text{ m} \Rightarrow \boxed{\lambda_s = 85 \text{ cm}}$$

## Problem 5



$$80^\circ\text{C} = 353\text{K}$$

$$90^\circ\text{C} = 363\text{K}$$

Water has molecular weight 18  $\Rightarrow$  1 mol = 18 g =  $18 \cdot 10^{-3}$  kg

At  $80^\circ\text{C}$ ,  $P = 4.73 \times 10^4 \text{ N/m}^2$ . Using  $PV = nRT$ ,  $\Rightarrow$

$$n = \frac{PV}{RT} = \frac{4.73 \times 10^4 \times 1.5}{8.314 \times 353} = \boxed{24.175 \text{ mols of steam initially}}$$

(b) At  $90^\circ\text{C}$ , if there is equilibrium between liquid and steam

$P = 7.01 \times 10^4 \frac{\text{N}}{\text{m}^2} \Rightarrow$  the number of mols of steam is

$$n = 24.175 \times \frac{7.01}{4.73} = 35.83 \text{ mol} \Rightarrow \text{requires}$$

$35.83 - 24.175 = 11.65$  extra mols, but we have only 10  $\Rightarrow$

all liquid evaporated  $\Rightarrow$  pressure is smaller.

$$(c) P = \frac{nRT}{V} = \frac{34.175 \times 8.134 \times 363}{1.5} \frac{\text{N}}{\text{m}^2} = \boxed{6.88 \times 10^4 \frac{\text{N}}{\text{m}^2}}$$

(d) The heat in raising the T from  $80^\circ\text{C}$  to  $90^\circ\text{C}$  is

$$Q = 3000 \frac{\text{J}}{\text{kg}^\circ\text{C}} \times 34.175 \text{ mol} \times 18 \times 10^{-3} \frac{\text{kg}}{\text{mol}} \times 10^\circ\text{C} = \boxed{18,454 \text{ J}}$$

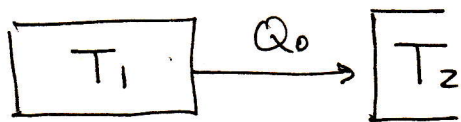
$$\text{Heat of vaporization } Q_v = 2.26 \times 10^6 \frac{\text{J}}{\text{kg}} \times 10 \text{ mol} \times 18 \cdot 10^{-3} \frac{\text{kg}}{\text{mol}} =$$

$= 406,800 \text{ J}$ . Since  $Q_v \gg Q$ , ignore  $Q$

$$\Delta S \sim \frac{Q_v}{T} = \frac{406,800 \text{ J}}{358 \text{ K}} = 1136 \frac{\text{J}}{\text{K}}$$

$T$  is the average temperature, ok as an approximation

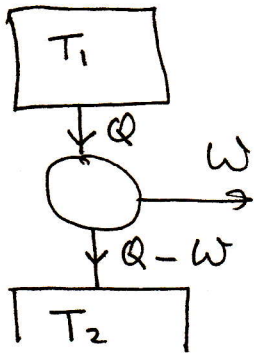
# Problem 6



$$Q_0 = C(T_1 - T_2) \Rightarrow$$

$$C = \frac{Q_0}{T_1 - T_2} \text{ is heat capacity of the body}$$

With a heat engine



As the heat engine runs, the body's temperature gradually decreases. The change in entropy of the body is

$$\Delta S_b = \int \frac{dQ}{T} = \int_{T_1}^{T_2} \frac{C dT}{T} = C \ln \frac{T_2}{T_1} \Rightarrow$$

$$\Delta S_b = -C \ln \frac{T_1}{T_2} = -\frac{Q_0}{T_1 - T_2} \ln \frac{T_1}{T_2}$$

The total work done after many cycles is  $W$ , the total heat transferred to the heat reservoir is  $Q_0 - W$   $\Rightarrow$  its entropy change is

$$\Delta S_r = \frac{Q_0 - W}{T_2} \text{ since its temperature doesn't change.}$$

If the engine is reversible,  $\Delta S_b + \Delta S_r = 0 \Rightarrow$

$$\Rightarrow \frac{Q_0 - W}{T_2} - \frac{Q_0}{T_1 - T_2} \ln \frac{T_1}{T_2} = 0 \Rightarrow Q_0 - W - \frac{Q_0 T_2}{T_1 - T_2} \ln \frac{T_1}{T_2} = 0 \Rightarrow$$

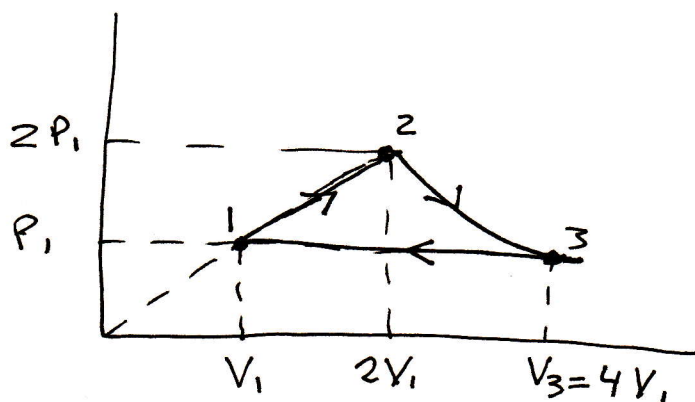
$$\Rightarrow W = Q_0 \left( 1 - \frac{T_2}{T_1 - T_2} \ln \frac{T_1}{T_2} \right) \Rightarrow \frac{W}{Q_0} = 1 - \frac{1}{\frac{T_1}{T_2} - 1} \ln \frac{T_1}{T_2}$$

that's the maximum, if engine is irreversible,  $\Delta S > 0$  and  $W/Q_0$  is smaller.

$$(b) \text{ For } \frac{W}{Q_0} = 0.5 = \frac{1}{2} \Rightarrow \frac{1}{2} = \frac{1}{\frac{T_1}{T_2} - 1} \ln \frac{T_1}{T_2} \Rightarrow \frac{T_1}{T_2} = 1 + 2 \ln \frac{T_1}{T_2}$$

Solving by iteration,  $\frac{T_1}{T_2} \approx 3.5$ , so range of possible values is  $\frac{T_1}{T_2} \geq 3.5$  ( $>$  if engine is irreversible)

## Problem 7



(a) Process 1-2

$$P_1 V_1 = n R T_1 ; P_2 V_2 = 4 P_1 V_1 = n R T_2 \Rightarrow \boxed{T_2 = 4 T_1}$$

$$\Delta E_{int} = C_v \Delta T = \frac{3}{2} n R \cdot 3 T_1 = \frac{9}{2} n R T_1$$

$$W = \frac{3}{2} P_1 \cdot (2V_1 - V_1) = \frac{3}{2} P_1 V_1 = \boxed{\frac{3}{2} n R T_1, \text{ did positive work}}$$

$$Q = \Delta E_{int} + W = \boxed{6 n R T_1, \text{ absorbed heat}}$$

(b) Process 2-3: isothermal, so  $\Delta E_{int} = 0$

$$W = \int_2^3 P dV = n R T_2 \ln \frac{V_3}{V_2} = 4 n R T_1 \ln \frac{V_3}{V_2} ; V_2 = 2V_1 ;$$

$$P_1 V_3 = n R T_2 = 4 n R T_1 \Rightarrow \boxed{V_3 = 4V_1} \Rightarrow \boxed{W = 4 n R T_1 \ln 2}$$

$$\boxed{Q = W = 4 n R T_1 \ln 2 \text{ absorbed}}$$

(c) Process 3-1 :  $W = -P_1 \cdot 3V_1 = -3 n R T_1$

$$\Delta E_{int} = C_v \Delta T = \frac{3}{2} n R (T_1 - 4T_1) = -\frac{9}{2} n R T_1 \Rightarrow$$

$$\boxed{Q = \Delta E_{int} + W = -\frac{15}{2} n R T_1, \text{ released}} \quad (n C_p \Delta T = -\frac{5}{2} n R \cdot 3T_1)$$

Total work:  $W_+ = \frac{3}{2} n R T_1 + 4 n R T_1 \ln 2 - 3 n R T_1 \Rightarrow$

$$\boxed{W_+ = (4 \ln 2 - \frac{3}{2}) n R T_1}$$

Total heat absorbed:  $Q_+ = 6 n R T_1 + 4 n R T_1 \ln 2 = \boxed{(4 \ln 2 + 6) n R T_1}$

Efficiency:

$$e = \frac{W_+}{Q_+} = \frac{4 \ln 2 - 3/2}{4 \ln 2 + 6} = 0.145$$

(e) Efficiency is low because a lot of heat is absorbed at lower temperatures and released at higher temperatures than the maximum ( $4T_1$ ) and minimum ( $T_1$ ) temperatures.

The best efficiency results when all the heat absorbed is at the highest temperature, and all the heat released is at the lowest temperature, which is the Carnot cycle

$$e_c = 1 - \frac{T_1}{4T_1} = 0.75 \gg 0.145$$

(f) For free expansion,  $\Delta S_{\text{gas}} = nR \ln \frac{V_f}{V_i} = nR \ln 2$  here.

Everything except this step is reversible in the cycle, and the change of entropy of the gas in 1 cycle is 0  $\Rightarrow$

$$\Delta S_{\text{univ}} = nR \ln 2$$

If the expansion is reversible the environment decreases its entropy by  $nR \ln 2$  in that process, in the free expansion instead the environment doesn't change its entropy.



### Problem 8

$E_A = \text{energy of system A}$ ,  $E_B = \text{energy of system B}$

$E_A + E_B = 3$ , A has 2 particles, B has 3 particles

$E_A$	$E_B$	microstates of A	#	microstates of B	#	total # of microstates	energy/particle in A	energy/particle in B
3	0	3,0 2,1 1,2 0,3	4	0,0,0	1	4	1.5	0
2	1	2,0 1,1 0,2	3	1,0,0 0,1,0 0,0,1	3	9	1	0.33
1	2	1,0 0,1	2	2,0,0 0,2,0 0,0,2 1,1,0 1,0,1 0,1,1	6	12	0.5	0.66
0	3	0,0	1	3,0,0 0,3,0 0,0,3 2,1,0 2,0,1 1,2,0 0,2,1 1,0,2 0,1,2 1,1,1	10	10	0	1

(b) The most likely partition is  $E_A = 1$ ,  $E_B = 2$ , for 12 microstates. The average energy per particle is 0.5 and 0.66 for A and B.

(c) Initially  $S = k \ln W_m = k \ln 4 = 1.39k$

At the end  $S = k \ln 12 = 2.48k$

$$\Rightarrow \Delta S = 1.10k > 0$$