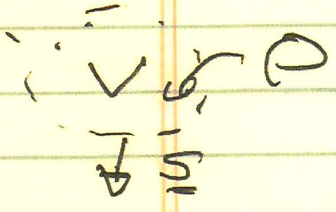


Physics 216

Lecture II - Ideal Fluids

- Equations
- Basic Concepts - especially } Helmholtz's Thm.
- Induced Mass, Quasi (Pseudo) Momentum } potential flow

I.) Euler Equations / Ideal Fluids. "The Flow of Dry Water" - RWF



Volume V
density ρ

argue microscopically but really derive from Boltzmann Eqn.

- Mass conservation:

$$\frac{dM}{dt} = \frac{d}{dt} \int d^3x \rho(\underline{x}, t) = - \int d^3x [\underline{v} \cdot \rho]$$

$$= - \int d^3x \underline{v} \cdot (\rho \underline{v})$$

so

$$\boxed{\partial_t \rho + \underline{v} \cdot (\rho \underline{v}) = 0}$$

continuity

$$\partial_t \rho + \underline{v} \cdot \underline{\Gamma} = 0$$

$$\underline{\Gamma} = \rho \underline{v}$$

mass flux density

- Momentum conservation:

ρ
 Fluid element

$$\underline{F} = - \underline{\nabla} p + \underline{F}$$

Net force density on element

pressure gradient

body force
 $(\underline{J} \times \underline{B}) / c$
 (in MHD)

So, Sir Isaac:

$$\rho \underline{a} = - \underline{\nabla} p + \underline{F}$$

acceleration

$$\underline{a} = \frac{d\underline{v}}{dt}$$

what does this mean (substantive derivative)

here:

→ increment in \underline{v}

displ.
↓

$$\underline{dv} = \frac{\partial \underline{v}}{\partial t} dt + d\underline{r} \cdot \underline{\nabla} \underline{v}$$

velocity increment

local acceleration

(particle moves/displaced in inhomogeneous velocity field.)

$$\frac{d\underline{v}}{dt} = \frac{\partial \underline{v}}{\partial t} + \frac{d\underline{m}}{dt} \cdot \underline{\nabla} \underline{v}$$

$$= \frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \underline{\nabla} \underline{v}$$

⇒

$$\rho \frac{d\underline{v}}{dt} = \rho \left(\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \underline{\nabla} \underline{v} \right) = -\underline{\nabla} p + \underline{F}$$

Euler Egn.

⌈ Momentum Flux ⌋

$$\partial_t (\rho v_i) = - \frac{\partial \Pi_{ik}}{\partial x_k}$$

i.e.

$$\partial_t (\rho \underline{v}) = \underline{v} \partial_t \rho + \rho \frac{\partial \underline{v}}{\partial t}$$

momentum density

$$= -\underline{v} \left(\rho (\underline{\nabla} \cdot \underline{v}) + \underline{v} \cdot \underline{\nabla} \rho \right)$$

$$+ \rho \left(-\underline{v} \cdot \underline{\nabla} \underline{v} - \frac{\underline{\nabla} p}{\rho} \right)$$

$$= - \left(\rho \left[\underline{v} (\underline{\nabla} \cdot \underline{v}) + \underline{v} \cdot \underline{\nabla} \underline{v} \right] + \underline{v} (\underline{v} \cdot \underline{\nabla} \rho) \right) - \underline{\nabla} p$$

$$= -\underline{\nabla} \cdot (\rho \underline{v} \underline{v} + \underline{\underline{I}} P)$$

\downarrow
Reynolds stress tensor
identity tensor

\rightarrow analogous to Maxwell stress tensor

so

$$\pi_{ik} = \rho v_i v_k + \delta_{ik} P$$

and

$$\frac{\partial}{\partial t} \int d^3x \rho \underline{v} = \frac{d}{dt} \underline{P} = -\int dS \cdot (\rho \underline{v} \underline{v} + \underline{\underline{I}} P)$$

$\pi_{ik} dS_k \equiv$ momentum flux in i th direction.

$$\pi_{ik} = \rho v_i v_k + \delta_{ik} P.$$

defines
momentum
flux

- in N-S. Eqn, viscous stress appears due momentum flux from collisions, interacting with macroscopic flow gradients

→ Mass, Momentum and Energy!

In ideal fluid, no heat exchanged between fluid elements ⇒ motion adiabatic - i.e. entropy conserved along trajectories

$$\frac{dS}{dt} = 0$$

$S \equiv$ entropy per mass.

$$\Rightarrow \boxed{\frac{\partial S}{\partial t} + \underline{v} \cdot \nabla S = 0}$$

adiabatic equation for fluid.

For energy Flux:

$$\mathcal{E} = \rho \frac{v^2}{2} + \rho E$$

\downarrow total energy density of fluid element
 \downarrow kinetic energy density
 \rightarrow internal energy density (i.e. thermal)

Now, as with momentum, consider

$$\frac{\partial \mathcal{E}}{\partial t};$$

$$\frac{\partial \mathcal{E}}{\partial t} = \frac{\partial}{\partial t} \left(\rho \frac{v^2}{2} + \rho E \right)$$

$$\frac{\partial}{\partial t} \left(\frac{\rho V^2}{2} \right) = \frac{V^2}{2} \frac{d\rho}{dt} + \rho \underline{V} \cdot \frac{\partial \underline{V}}{\partial t}$$

$$= - \frac{V^2}{2} \underbrace{\underline{D} \cdot (\rho \underline{V})}_{\text{cont.}} - \underbrace{\underline{V} \cdot \underline{D} P}_{\substack{\text{momentum} \\ \text{balance}}} - \rho \underline{V} \cdot (\underline{V} \cdot \underline{D} \underline{V})$$

$$\underline{V} \cdot \underline{D} \underline{V} = - \underline{V} \times \underline{\omega} + \frac{1}{2} \underline{D} (V^2)$$

$\underline{\omega} = \underline{D} \times \underline{V} \rightarrow$ vorticity

18

$$\rho \underline{V} \cdot (\underline{V} \cdot \underline{D} \underline{V}) = \rho \underline{V} \cdot \left(- \underline{V} \times \underline{\omega} + \underline{D} \left(\frac{V^2}{2} \right) \right)$$

$$= \rho \underline{V} \cdot \underline{D} \frac{V^2}{2}$$

and

$$dW = dE + d(PV)$$

enthalpy = $T ds + v dp$

$$= T ds + \frac{dp}{\rho}$$

so

$$\underline{D} P = \rho \underline{D} W - \rho T \underline{D} S$$

thus, ①

$$\frac{d}{dt} \left(\frac{\rho V^2}{2} \right) = -\frac{V^2}{2} \underline{\underline{D}} \cdot (\underline{\rho V}) - \rho \underline{V} \cdot \underline{D} \left(\frac{V^2}{2} + w \right) + \rho T \underline{V} \cdot \underline{D} \underline{\rho}$$

For ②:

$$\frac{d}{dt} (\rho \epsilon) =$$

Useful to transform using thermodynamic identity:

$$\begin{aligned} d\epsilon &= dQ - p dV \\ &= T ds - p dV \end{aligned}$$

but $V = 1/\rho$

$$dV = -d\rho/\rho^2$$

$$d\epsilon = T ds + \frac{p}{\rho^2} d\rho$$

$$\underline{\underline{so}} \quad d(\rho \epsilon) = \rho d\epsilon + \epsilon d\rho$$

1st

$$d(\rho E) = \left(\frac{\rho}{\rho} + E \right) d\rho + \rho T ds$$

$$E + \frac{p}{\rho} = E + \rho v = w$$

↓
enthalpy

2nd

$$d(\rho E) = w d\rho + \rho T ds$$

$$\textcircled{2} \quad \frac{\partial}{\partial t} (\rho E) = w \frac{\partial \rho}{\partial t} + \rho T \frac{\partial s}{\partial t}$$

$$= -w \underline{D} \cdot (\rho \underline{v}) - \rho T \underline{v} \cdot \underline{D} s$$

So, combining 1, 2:

$$\frac{\partial}{\partial t} \left(\rho \frac{v^2}{2} + \rho E \right) = \frac{-v^2}{2} \underline{D} \cdot (\rho \underline{v}) - \rho \underline{v} \cdot \underline{D} \left(\frac{v^2}{2} + w \right) - w \underline{D} \cdot (\rho \underline{v}) - \rho T \underline{v} \cdot \underline{D} s + \rho T \underline{v} \cdot \underline{D} s$$

$$= - \left(\frac{v^2}{2} + w \right) \underline{D} \cdot (\rho \underline{v}) - \rho \underline{v} \cdot \underline{D} \left(\frac{v^2}{2} + w \right)$$

$$= - \underline{D} \cdot \left(\rho \underline{v} \left(\frac{v^2}{2} + w \right) \right)$$

Thus, have:

$$\frac{\partial}{\partial t} \left(\frac{\rho V^2}{2} + \rho E \right) + \underline{\nabla} \cdot \left(\rho \underline{V} \left(\frac{V^2}{2} + w \right) \right) = 0$$

so

$$\frac{\partial}{\partial t} \int_V d^3x \left(\frac{\rho V^2}{2} + \rho E \right) = - \int d\underline{s} \cdot \left[\rho \underline{V} \left(\frac{V^2}{2} + w \right) \right]$$

↓ change in energy in volume V
 ↓ energy flux density thry surface.

energy density flux

$$\underline{Q} = \rho \underline{V} \left(\frac{V^2}{2} + w \right)$$

accompanies $\underline{\pi}_{ijk}, \underline{D}$

→ Meaning:

$$w = E + \frac{p}{\rho}$$

so

$$\int d\underline{s} \cdot \underline{Q} = \int d\underline{s} \cdot \rho \underline{V} \left(\frac{V^2}{2} + E \right) + \int d\underline{s} \cdot \rho \underline{V} \frac{p}{\rho}$$

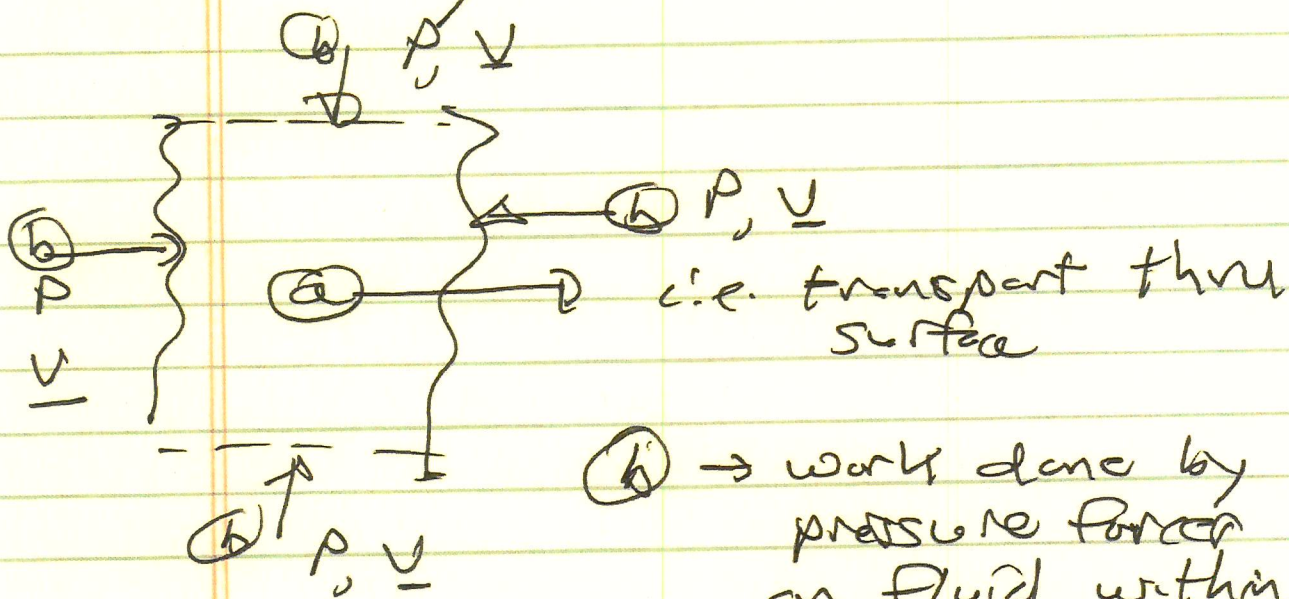
(a) Flux of KE and internal energy thry surface
(b)

$$\textcircled{b} = \int d\underline{s} \cdot \underline{v} P$$

$$= \int (\underline{v} \cdot d\underline{s}) P$$

↓
dV/dt

→ PdV work done by pressure forces on fluid within surface.



→ work done by pressure forces on fluid within S.

II.) Basic Concepts

Now, convenient to note:

$$dE = dQ - pdv$$

$$= Tds - pdv$$

$$W = E + pV$$

→ enthalpy as
Legendre transform
of entropy

then

$$dW = Tds + vdp$$

$$= Tds + \frac{dv}{\rho}$$

so, for isentropic motions ($ds = 0$),

$$dp/\rho = dW \quad \text{or} \quad \frac{\nabla p}{\rho} = \nabla W$$

→ has advantage of RHS of Euler Eqn. as perfect derivative,

$$\frac{\partial v}{\partial t} + v \cdot \nabla v = \frac{dv}{dt} = -\nabla W$$

Then, can immediately note:

$$\frac{d}{dt} \oint \underline{v} \cdot d\underline{l} = 0$$

→ Circulation
conserved for
inviscid, isentropic
fluid

i.e.

$$\frac{d}{dt} \oint \underline{v} \cdot d\underline{l} = \oint \frac{d\underline{v}}{dt} \cdot d\underline{l}$$

↓
Kelvin's Thm.

$$+ \oint \underline{v} \cdot \frac{d d\underline{l}}{dt}$$

$$= \oint \frac{d\underline{v}}{dt} \cdot d\underline{l} + \oint \underline{v} \cdot \frac{d d\underline{l}}{dt}$$

$$= \oint (-\underline{\nabla} w) \cdot d\underline{l} + \oint \underline{v} \cdot d\underline{v}$$

$$= 0 + 0$$

i.e.

$$\oint \underline{v} \cdot d\underline{l} = \text{const}$$

For closed
contour
in ideal,
isentropic
fluid

often:

Note: no use
 $\nabla \cdot \underline{v} = 0$

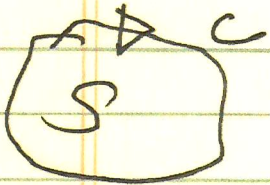
$$\Gamma = \oint \underline{v} \cdot d\underline{l}$$

→ conserved,
(absolute)

N.B.: obvious analogy in mechanics
is Poincaré-Cartan invariant.

$$I_{PC} = \oint \underline{p} \cdot d\underline{q}$$

$$\frac{d}{dt} I_{PC} = 0$$



for Hamiltonian
system.

Now, elementary vector calc. →
normal to enclosed
area.

$$\Gamma = \oint_C \underline{v} \cdot d\underline{l} = \int_A \underline{\omega} \cdot d\underline{S} \rightarrow \text{const.}$$

$$\underline{\omega} = \nabla \times \underline{v}$$

Vorticity

What is vorticity?

→ describes rotation of
fluid element.

→ ω is 2ω effective local angular velocity of fluid

i.e. $\underline{dV} = (\underline{\omega} \times \underline{r})/2$

→ vorticity is the non-trivial element in fluid dynamics, beyond Bernoulli's Law and potential flow. Vorticity is central to all interesting topics.

Now,

$$\frac{\partial \underline{V}}{\partial t} + \underline{V} \cdot \nabla \underline{V} = -\nabla W$$

$$\begin{aligned} \underline{V} \cdot \nabla \underline{V} &= -\underline{V} \times (\nabla \times \underline{V}) + \nabla \frac{V^2}{2} \\ &= -\underline{V} \times \underline{\omega} + \nabla \frac{V^2}{2} \end{aligned}$$

$\nabla \times$

Magnus Force

$$\frac{\partial \underline{V}}{\partial t} - \underline{V} \times \underline{\omega} = -\nabla \left(W + \frac{V^2}{2} \right)$$

then $\nabla \times$

⇒ Ideal vorticity (Induction) equation:

$$\frac{\partial \underline{\omega}}{\partial t} = \nabla \times (\underline{v} \times \underline{\omega})$$

$$= -\underline{v} \cdot \nabla \underline{\omega} + \underline{\omega} \cdot \nabla \underline{v} - \underline{\omega} \nabla \cdot \underline{v}$$

$$\frac{d\underline{\omega}}{dt} = \underline{\omega} \cdot \nabla \underline{v} - \underline{\omega} \nabla \cdot \underline{v}$$

or, with continuity:

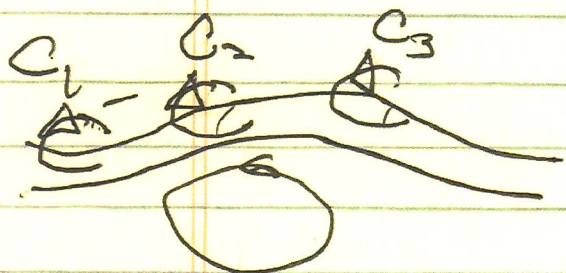
$$\frac{d}{dt} \frac{\underline{\omega}}{\rho} = \frac{\underline{\omega}}{\rho} \cdot \nabla \underline{v}$$

→ "frozen-in"

→ can derive Kelvin's Theorem from induction equation

→ viscosity breaks circulation conservation.

III.) Potential Flow



excludes case
of separation!

- Consider fluid streamlines

i.e. streamlines are lines along which fluid flows, i.e.

$$\frac{dx}{u_x} = \frac{dy}{u_y} = \frac{dz}{u_z}$$

then if $\underline{\omega} = 0$ at any point on streamline, Kelvin's theorem $\Rightarrow \underline{\omega} = 0$ everywhere on line

i.e. Easily seen by considering "circulation" around infinitesimal loop "pulled" along line. Thus if:

$$\oint_{C_1} \underline{u} \cdot d\underline{l} = \int_{A_1} \underline{\omega} \cdot d\underline{s} = 0, \text{ then}$$

$$\oint_{C_n} \underline{u} \cdot d\underline{l} = \int_{A_n} \underline{\omega} \cdot d\underline{s} = 0, \text{ all } C_n$$

- Flow with $\underline{\omega} = 0 = \underline{\sigma} \times \underline{v}$ in
all space

\Rightarrow potential, irrotational flow.

$\rightarrow \underline{\omega} \neq 0 \rightarrow$ vortical rotation