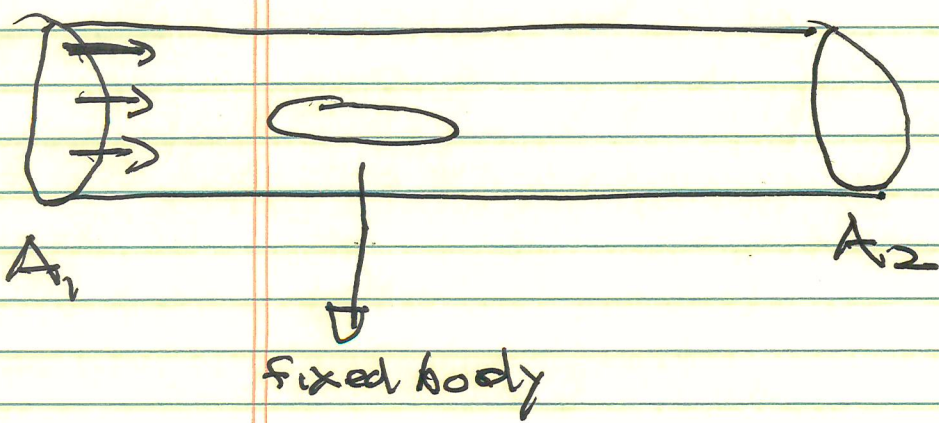


Lecture VII

Waves: Stability and Structure

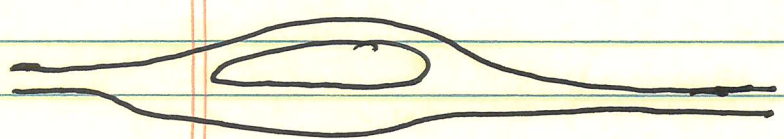
→ Recall D'Alembert's Paradox



Drag Force = Difference in Momentum Flux thru ends

$$F_d = \int_{A_1} da_1 (P_1 + \rho V_1^2) - \int_{A_2} da_2 (P_2 + \rho V_2^2)$$

- For ~~inviscid~~ ideal fluid, upstream/downstream symmetry of flow



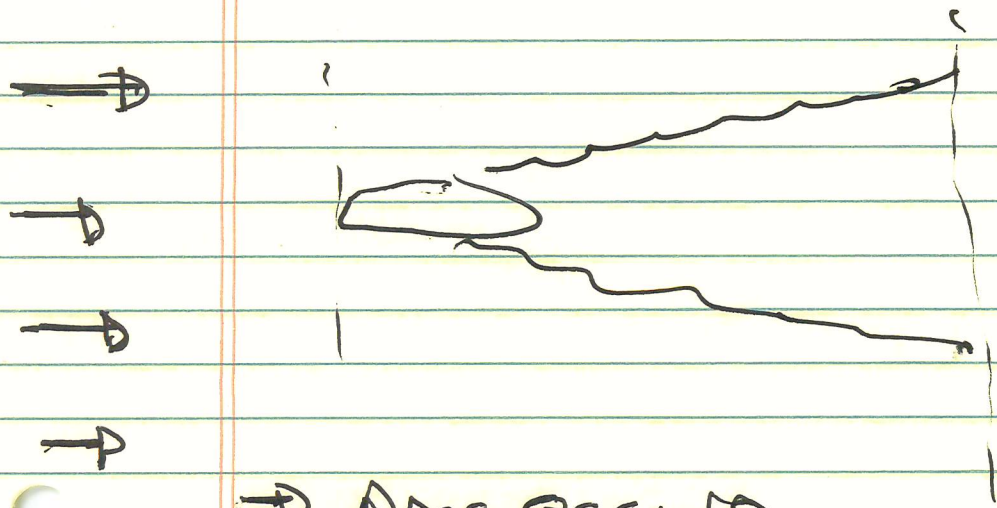
i.e. $P_1 = P_2$
 $V_1 = V_2$

∴ $F_d = 0$

i.e. effect of flow is enhanced inertia (induced mass)

- For viscous fluid (i.e. no slip boundary condition) \rightarrow upstream/downstream asymmetry

\rightarrow wake

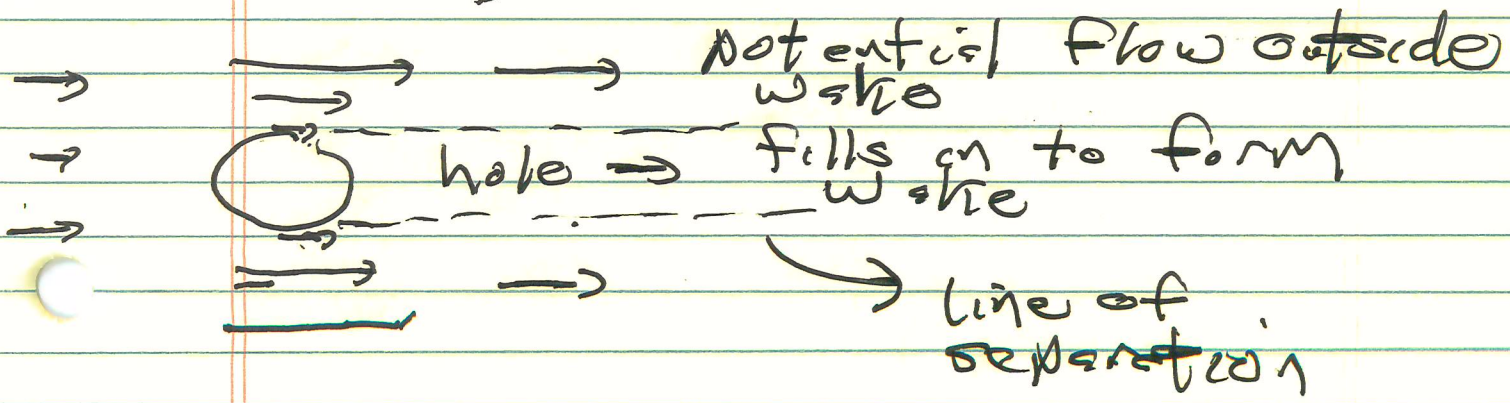


\Rightarrow Drag occurs

Aim is to understand structure and dynamics of wake.

\rightarrow Recall: No-slip B.C.'s

\rightarrow Separation occurs



- wake is rotational / vortices
for $Re > Re_{crit}$

- how does hole fill in?

①

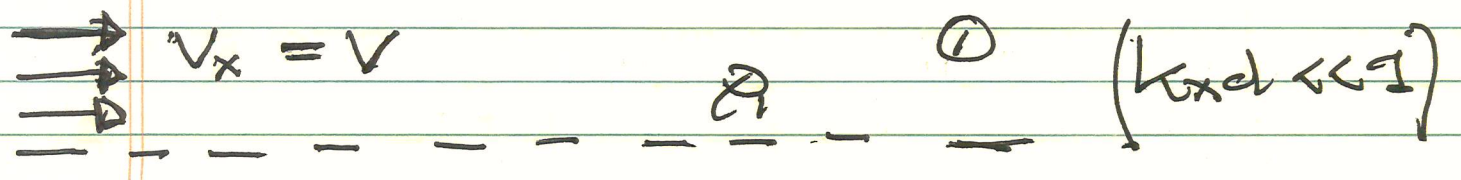
⇒ Separation is unstable

⇒ Kelvin-Helmholtz Instability

KH

→ free energy → DV

- simplification: interface



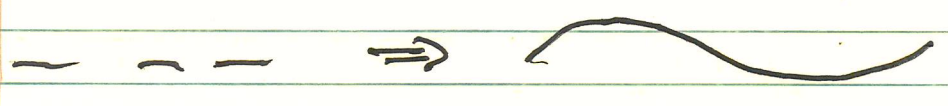
$v_x = 0$ ρ_2 ②

- DV = 0, except interface

- $\omega = \partial v_x / \partial z = 0$, except interface

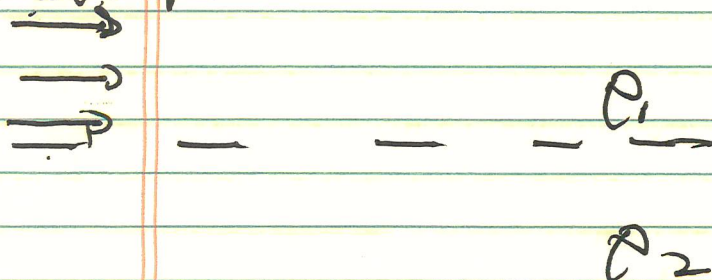
- can treat as potential flow
in regions ①, ② and match
at interface

- interface ripples → dynamic b.c.



Physical ideas:

① critical

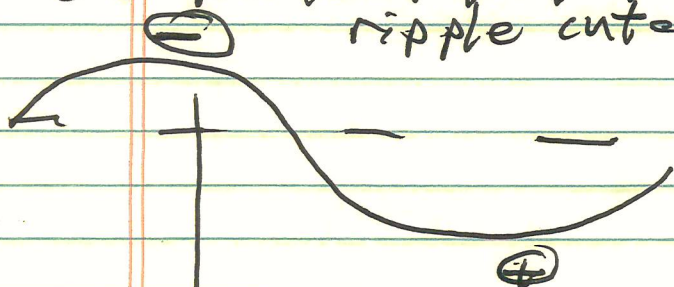


① high v , low p

② zero v , high p

② ∂v perturbation \rightarrow ripple interface

$$\rho + \frac{\rho v^2}{2} = \text{const.}$$



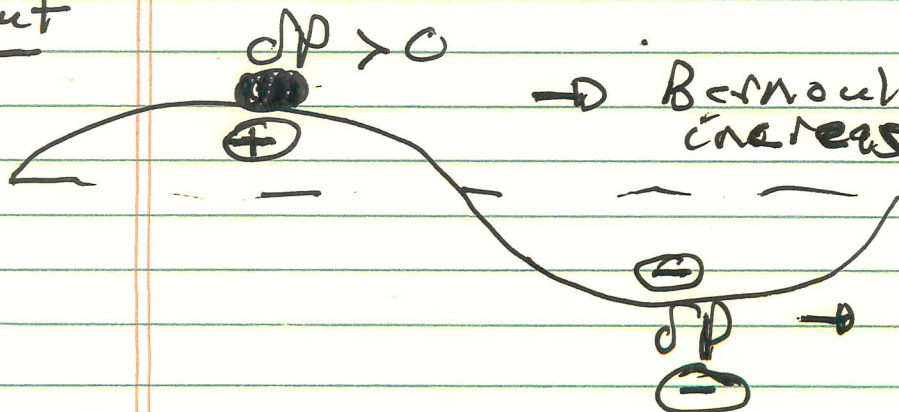
$$\partial v_1 < 0$$

- ripple brings in slow fluid
- flow in region ① drops

$$\partial v_2 > 0$$

- ripple brings in fast fluid
- flow in ② increases

but



\rightarrow Bernoulli \Rightarrow pressure increases

pressure decreases

$\frac{d\rho}{\rho} > 0 \Rightarrow dV < 0$ further
 $\frac{d\rho}{\rho} < 0 \Rightarrow dV > 0$ further

reinforcing initial perturbation!

N.B. K-H instability drives viscous mixing via turbulence, mixing, billows etc.

To calculate:

ρ_1
 ρ_2

$\rho + \rho_1 \frac{v^2}{2} = \text{const}$
 assumed equilibrium

PE

$$\nabla \cdot \underline{v} = 0$$

$$\underline{v} = \nabla \phi$$

$\underline{\omega} = 0$, except interface

$$\nabla^2 \phi = 0$$

$(\partial_z^2 - k^2) \phi = 0$
 wave along interface (symmetry)

$$\phi = \sum_k \phi_k e^{ikx} e^{-k|z|} e^{-i\omega_k t}$$

decays away from interface

matching conditions

→ pressure continuity

$$\tilde{p}_1(z_1) = \tilde{p}_2(z_2)$$

→ ϕ continuity

i.e. $-\rho = \rho \partial_t \phi + \rho \frac{(\nabla \phi)^2}{2}$

→ $\left. \frac{\partial \phi}{\partial z} \right|_{\text{①}} = \left. \frac{\partial \phi}{\partial z} \right|_{\text{②}}$

i.e. $\partial_z^2 \phi - k^2 \phi = 0$

and $\int_{z_-}^{z_+} \partial_z^2 \phi = 0 \Rightarrow \left. \partial_z \phi \right|_{z_+} - \left. \partial_z \phi \right|_{z_-} = 0$

Now,

$$\partial_t \underline{v} + \underline{v} \cdot \nabla \underline{v} = -\frac{\nabla p}{\rho}$$

$$\rho_1 (\partial_t \tilde{v}_{z_1} + v \partial_x \tilde{v}_{z_1}) = -\partial_z \tilde{p}_1$$

$$\rho_2 (\partial_t \tilde{v}_{z_2}) = -\partial_z \tilde{p}_2$$

$$\underline{\text{So}} \quad \tilde{v}_{z_1} = \frac{-ck \tilde{P}_1}{\rho_1 (kv - \omega)}$$

$$\tilde{v}_{z_2} = \frac{ck \tilde{P}_2}{-\rho_2 \omega}$$

$$\rho_2 \tilde{P}_2 \begin{cases} - \text{①} \\ + \text{②} \end{cases}$$

(not related v_z)

Now, dynamic boundary:

$$\eta = \eta(x, t) \rightarrow \text{displacement}$$

$$\frac{d\eta}{dt} = \tilde{v}_{z_1}$$



and

$$\partial_t \tilde{\eta} + v \partial_x \tilde{\eta} = \frac{d\tilde{\eta}}{dt}$$

$$-c(\omega - kv) \tilde{\eta}_k = \tilde{v}_{z_1, k}$$

⇒

$$-c(\omega - kv) \tilde{\eta}_k = \frac{-ck \tilde{P}_1}{\rho_1 (kv - \omega)}$$

$$\tilde{P}_{1, k} = -\rho_1 \frac{(kv - \omega)^2}{k} \tilde{\eta}_k$$

$$\tilde{P}_2 = \rho_2 \frac{\omega^2}{k} \tilde{N}_k$$

and $\tilde{P}_1 = \tilde{P}_2 \Rightarrow$

$$-\frac{\rho_1}{k} (kv - \omega)^2 = \frac{\rho_2 \omega^2}{k}$$

and finally,

$$\omega = kv \left(\frac{\rho_1 + i(\rho_1 \rho_2)^{1/2}}{\rho_1 + \rho_2} \right)$$

$$\rightarrow \gamma \sim \frac{kv(\rho_1 \rho_2)}{\rho_1 + \rho_2}$$

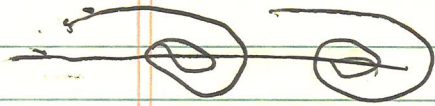
$$\rightarrow \omega_{\text{real}} \sim kv \left[\frac{\rho_1}{(\rho_1 + \rho_2)} \right]$$

\Rightarrow no exchange of stabilities here.

$$\rightarrow \rho_1 = \rho_2, \quad \gamma \sim kAV$$

→ What happens?

→ vortex roll-up, billows



(see Falkovich
F 2.3, F 2.4)

→ Vortex streets etc.

→ N.B. Vorticity concentrated in layer of interface.

→ More generally:

$$\gamma^2 = \frac{\rho_1 \rho_2}{(\rho_1 + \rho_2)^2} k^2 (v_2 - v_1)^2 + \frac{(\rho_1 - \rho_2)}{\rho_1 + \rho_2} (g/k)$$

(g > 0)

~~(g < 0)~~

$$- \frac{\gamma k^3}{(\rho_1 + \rho_2)}$$

↓
surface tension
→ (capillarity)

↓
Rayleigh-Taylor

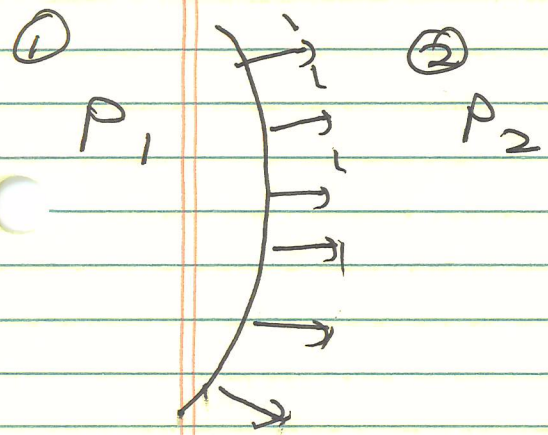
~ Threshold wind to excite waves

Surface Tension

- An important property of interface is surface tension

i.e. - Force due to crease in surface area of interface

- Familiar from droplets, capillary waves, etc.



isothermal displacement, as
 1 expands
 1 expands into 2

$$dF = -P_1 dV - P_2 (-dV) + \gamma dA$$

\uparrow
 1 expands into 2

\downarrow
 2 contracts

\downarrow
 change in free energy

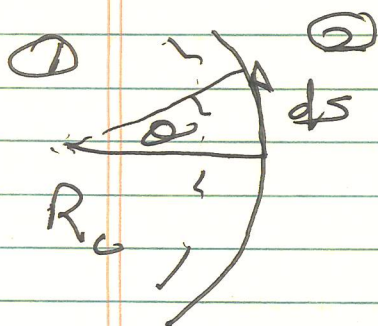
∞, criterion for equilibrium:

$$p_2 - p_1 = \gamma \nabla^2 \eta$$

$$dF = (p_2 - p_1) dA d\eta + \gamma dA$$

More generally:

Now consider (i.e. not "weakly curved" interface)



$$ds = (R_c + d\eta) d\theta = d\ell_0 \left(1 + \frac{d\eta}{R_c} \right)$$

radius curvature of interface, as shown

In general, surface parametrized by 2 radii curvature; R_1, R_2 (Gauss):

$$dA = \int dl_1 dl_2 \left(1 + \frac{d\eta}{R_1} \right) \left(1 + \frac{d\eta}{R_2} \right)$$

$$- \int dl_1 dl_2$$

$$= \int dl_1 dl_2 \left(\frac{1}{R_1} + \frac{1}{R_2} \right) d\eta$$

$$\frac{dF}{dV}$$

$$dF = \int dA_0 \left[(P_2 - P_1) + \gamma \left(\frac{1}{R_1} + \frac{1}{R_2} \right) \right] dV$$

Eq., far equilibrium with interface (general)

$$\gamma \left(\frac{1}{R_1} + \frac{1}{R_2} \right) = P_1 - P_2$$

LAPLACE'S LAW

N.B.:

→ Given 2-phase equilibrium (separate domains), can use Laplace Law to estimate droplet size for immiscible liquids

d.e. $P_1 > P_2$, $R \approx \frac{\gamma}{(P_1 - P_2)}$

→ For SW, $R = T$

$$P \rightarrow P = \rho \gamma_T \frac{1}{R^2} \dots \frac{\rho_L}{\rho_H} \frac{\gamma_T}{\rho_H}$$

$$W^2 = \frac{\rho_H - \rho_L}{\rho_H + \rho_L} \gamma_T + \frac{\gamma_T^3}{(\rho_H + \rho_L)}$$

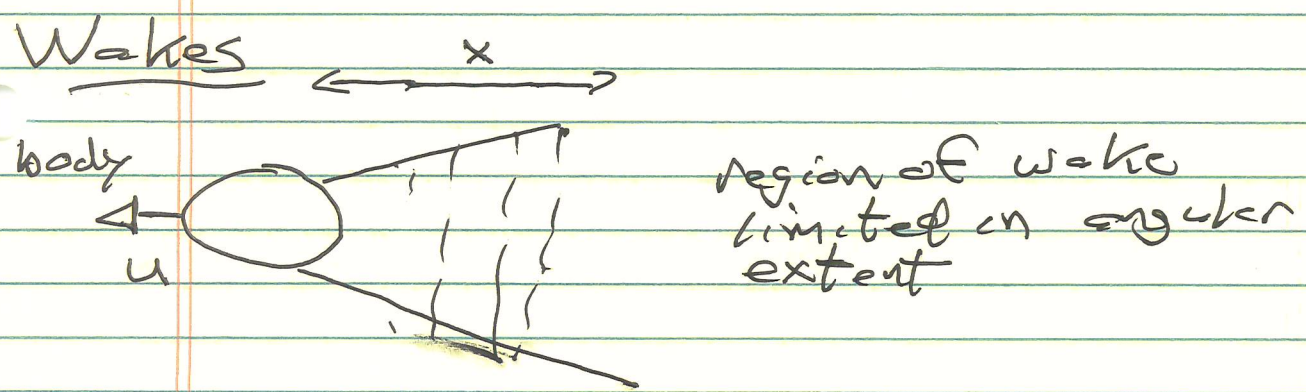
For $\rho_H \gg \rho_L$

$$\omega^2 = \underbrace{gk}_{\text{gravity wave}} + \underbrace{\frac{\gamma}{\rho}}_{\text{cap.}} k^3 \quad \rightarrow \text{Grev-} \\ \text{capillary wave}$$

- cross-over at few cm.
capillary effects important at $\leq 5 \text{ cm}$.

→ Wake Structure

- Physics ideas → wake flow created by response to separation
- Link: Drag - asymmetry - wake flow
- width: Laminar, Turbulent
Scales
- ~~Deficit~~ Deficit and punchline re:
N-S vs Euler



- region behind body of departure from potential flow.
Wake rotational,

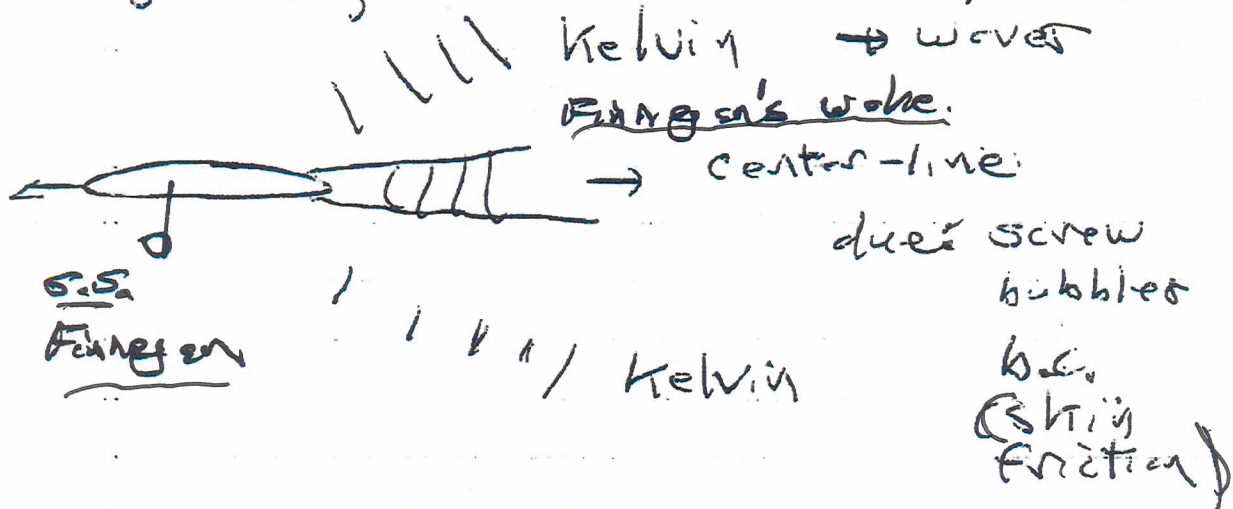
- ~~wake~~ wake breaks upstream-downstream symmetry of ideal flow

- wake is consequence of a body experiencing drag.

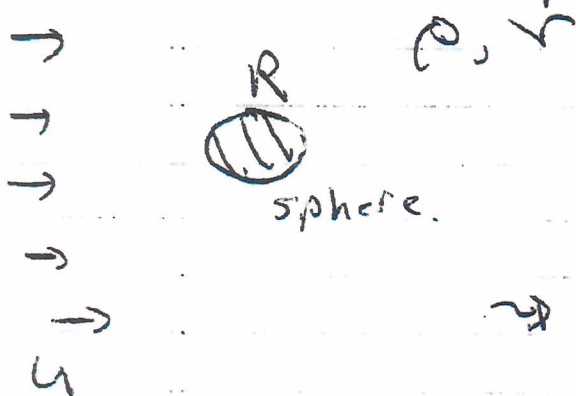
Message: A little viscosity forces a global adjustment in flow structure

Notes:

* - in general, wake multi-component



- here, consider spherical cow of wake problems.



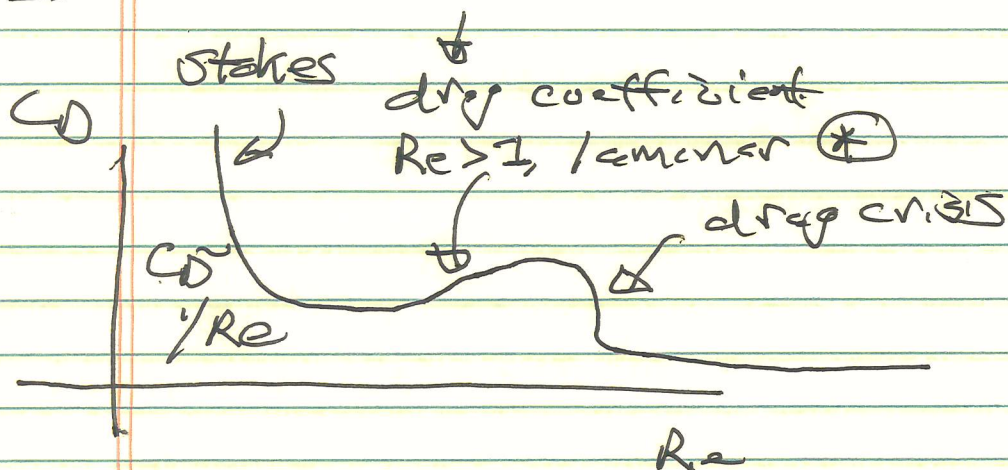
so $F_d \sim \rho U^2 R^2 f(R_c)$

no surface effects.

→ How calculate wake structure?

$$\text{Force of Drag} \equiv \left\{ \frac{\text{Rate of Net Momentum Loss from Flow}}{\rho U^2} \right\}$$

i.e. $F_d \sim C_D \rho A U^2$

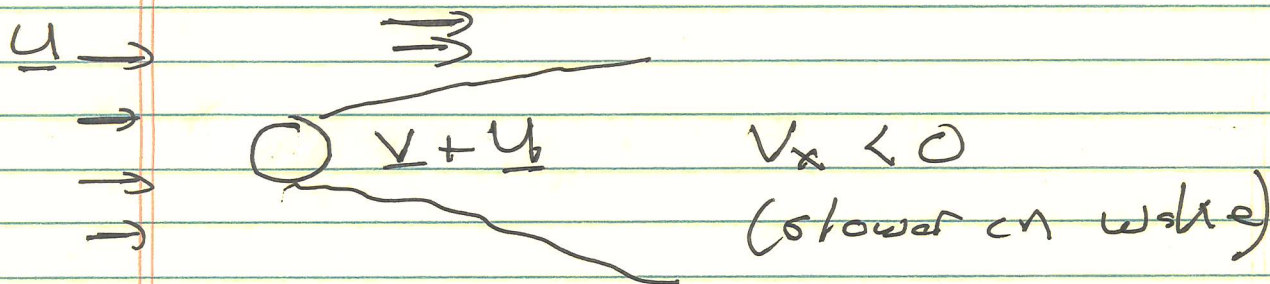


i.e. in laminar wake, flow not turbulent but inertia relevant

Further:

- distances behind body
 $x \gg R$, \rightarrow wake

- if body speed U , then in frame where body stationary,

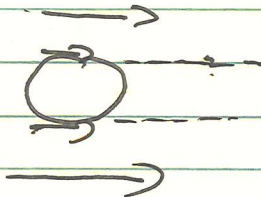


V differs zero in limited region

→ How limited? → as function, ↓ signal propagation is diffusion, only.

→ How does wake form?

→
→
→
→
→



- no slip boundary condition slows down fluid flowing past body

∴

- separation, discontinuity

but → left results, mixing fluid into hole

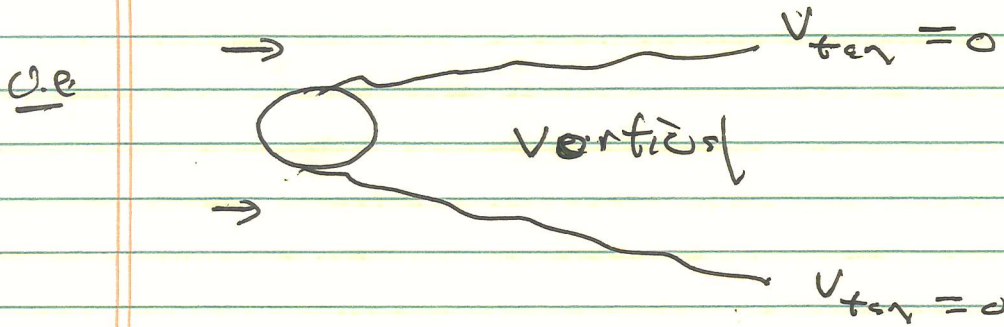
→ viscosity smooths out discontinuity

no. if turbulent wake turbulent mixing smooths discontinuity faster than viscous mixing.

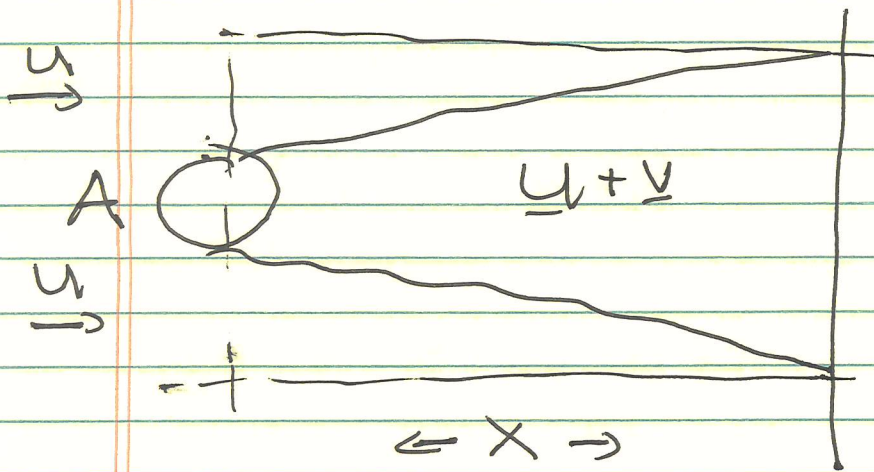
→ boundary of wake is traced by fluid particles

- passing close to body

- scattered by diffusion and turbulent mixing ⇒ expansion



Now, to calculate rate of loss of momentum from flow, return to D'Alembert's construction, but with asymmetry



$D_{res} =$
difference
influx, outflux

$$\underline{F}_d = \int_{A_0} d\underline{a} \cdot \underline{\Pi}_{tot}(0) - \int_{A_x} d\underline{a} \cdot \underline{\Pi}_{tot}(x)$$

$$\underline{\Pi} = p + \rho(\underline{u} + \underline{v})(\underline{u} + \underline{v})$$

$$\equiv p_{Tot.} \quad \rightarrow \text{Momentum Flux}$$

$$\Pi_{xx}(0) = p_0 + \rho U^2$$

i.e. $0(x)$

$$\int [p \delta_{in} + \rho U_i v_i] df_n$$

$$\Pi_{xx}(x) = p_0 + p' + \rho U^2 + \rho U v_x + h.o.$$

18

$$F_d \approx - \int_{A_w} da \rho U V_x$$

Now, can take considⁿ of symmetry, so

$$F_d \approx -\pi w(x)^2 \rho U V_x$$

What is width?

$V_x < 0$

$F_d > 0$

$\rightarrow \alpha$

Now, need $w(x)$ to get V_x !

\rightarrow Observe

- problem now reduced to one of scale.

- wakes self-similar.

$$w \sim x^\alpha, \quad \alpha ?$$

- wakes can be laminar or turbulent

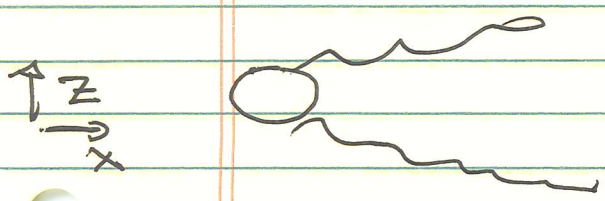
i.) laminar,

$$\frac{UR}{\nu} > 1$$

but not $\gg 1$

$$\frac{\partial \underline{V}}{\partial t} + \underline{V} \cdot \nabla \underline{V} - \nu \nabla^2 \underline{V} = -\frac{\partial p}{\partial x}$$

$$\underline{u} \cdot \nabla \underline{V} + \underline{v} \cdot \nabla \underline{V} - \nu \nabla^2 \underline{V} = -\frac{\partial p}{\partial x}$$



$\nabla \cdot \underline{V} = 0$
narrow wake

$$u \frac{\partial V_x}{\partial x} - \nu (\frac{\partial^2 V_x}{\partial x^2} + \frac{\partial^2 V_x}{\partial z^2}) = -\frac{\partial p}{\partial x}$$

$$u \frac{\partial V_x}{\partial x} - \nu \frac{\partial^2 V_x}{\partial z^2} = -\frac{\partial p}{\partial x}$$

$\frac{\partial x}{z} \sim 1/x$ downstream distance

$\frac{\partial z}{z} \sim 1/w$ \perp scale.

Obvious: $V \approx \frac{1}{(\frac{\nu x}{u})^{1/2}} \exp\left[-\frac{y^2}{\nu x/u}\right]$

$$\left(\frac{u}{x} - \frac{v}{w^2} \right) v_z \sim \frac{-\rho}{w^2}$$

$$\left(\frac{u}{x} - \frac{v}{w^2} \right) v_x \sim \frac{-\rho}{x^2}$$

$$\underline{\nabla} \cdot \underline{v} = 0 \quad \Rightarrow \quad \frac{v_x}{x} \sim \frac{v_z}{w}$$

as ρ negligible (will show) \Rightarrow

$$\frac{u}{x} \sim \frac{v}{w^2}$$

$$w \sim \left(\frac{vx}{u} \right)^{1/2}$$

\rightarrow diffusive spreading of momentum,
by v

$$\Rightarrow \sim (vt)^{1/2} \quad \text{with} \quad t \sim x/u$$

So

$$w \sim \left(\frac{x}{R} \right)^{1/2} \left(\frac{vR}{u} \right)^{1/2}$$

$$w/R \sim \left(\frac{x}{R} \right)^{1/2} / Re^{1/2}$$

- skin Blasius \checkmark

check: $\vec{z} \rightarrow$

$$15 \quad \frac{\rho}{\partial w} \sim \frac{r V_z}{w^2}$$

} ρ likely important
in V_z eqn.

$$\frac{V_x}{x} \sim \frac{V_x}{w}$$

$$\rho \sim \rho r \frac{V_x}{x}$$

$$\frac{\rho}{\partial x} \sim r \frac{V_x}{x^2}$$

but eqn. $\left(\frac{1}{x} - \frac{r}{w^2} \right) V_x \sim -\frac{\rho}{\partial x}$

$\left. \begin{array}{c} \{ \\ \mathcal{O}(1/w^2) \end{array} \right\} \quad \left. \begin{array}{c} \} \\ \mathcal{O}(1/x^2) \end{array} \right\}$

so drop ρ ✓

N.B. $\frac{\rho}{\partial w} \sim \frac{r}{w^2} V_z$

→ Some Observations re: Wakes

- $F_x = -\rho U \int_{wake} v_x dy dz$

⇒

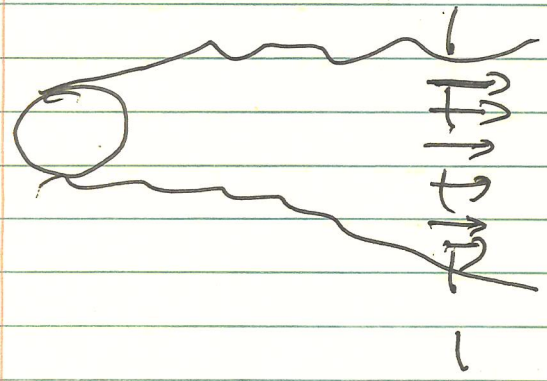
$Q = \rho \int_{wake} v_x dy dz$

net mass flow thru wake area

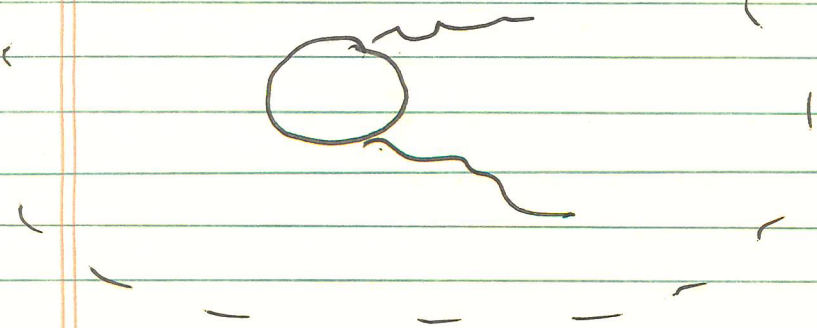
→ Wake deficit difference with/without body

Q is x independent:

c.e. $Q \sim F_x / U \rightarrow const$



but, if encircle body:



have:

$$\oint_{\text{tot}} \underline{v} \cdot d\underline{q} = 0$$

de. no
water lost

but

$$0 \equiv \int_{\text{wires}} \underline{v} \cdot d\underline{q} + \int_{\text{pot flow}} \underline{v} \cdot d\underline{q}$$

$$Q \sim v_x A$$

Q finite \Rightarrow

$$v_x \sim \frac{1}{A} \sim 1/r^2$$

so

$$\int_{\text{pot flow}} \underline{v} \cdot d\underline{q} = -Q$$

$$v_x A \sim -Q$$

$$v_x \sim 1/r^2$$

potential flow
monopole.

11/8

- Euler equation

$$v \sim 1/r^3 \rightarrow \text{dipole}$$

but for N-S eqn.

$$v \sim 1/r^2 \rightarrow \text{monopole}$$

⇒

- global adjustment in potential
Flow outside wake induced
by viscosity and the wake.

- Message: A little ν forces a
global adjustment in
flow structure.

by analogy with h.T. gases

$$\underline{v} \cdot \nabla \underline{v} \rightarrow -\nu_T \nabla^2 \underline{v}$$

$$\nu_T \sim \tilde{w} l_{mix}$$

(ii) Turbulent Wake

$Re \sim UR/\nu \gg 1$

$$\underline{u} \cdot \nabla \underline{v} + \underline{v} \cdot \nabla \underline{v} - \nu \nabla^2 \underline{v} = -\frac{\nabla p}{\rho}$$

$$\Rightarrow \frac{u}{x} v_x \sim \frac{\tilde{v}_y}{W} v_x$$

ignore

[wave spreads by advection, not diffusion]

$\tilde{v}_y \sim$ turbulent velocity

$$W \sim \frac{\tilde{v}_y x}{y}$$

Take wake turbulence isotropic

so $\tilde{v}_x \sim \tilde{v}_y$

{Fair? Test}

$W \sim x \tilde{v}_x / U$

but from drag:

$$\tilde{v}_x \sim F_d / \rho y W^2$$

\Rightarrow

118

$$W \sim x \frac{F_d}{\rho u^2 w^2} \sim x \left(F_d / \rho u^2 w^2 \right)$$

$$W^3 \sim F_d x / \rho u^2$$

$$\Rightarrow \boxed{W \sim (F_d / \rho u^2)^{1/3} x^{1/3} \\ \sim (C_D R^2)^{1/3} x^{1/3}}$$

then, comparing widths:

laminar: $w/R \sim (x/R)^{1/2} Re^{-3/2}$
 $Re \sim UR/\nu$

turbulent: $w/R \sim (x/R)^{1/3} C_D^{1/3}$

interestingly, laminar wake expands with downstream length more rapidly ↓

Why?

→ turbulence can relax ΔV behind object (due separation) rapidly, and faster than v . Thus surrounding flow penetrates the dead water region more rapidly, less wake expansion.

Also observe: Wake Re drops with

x

→

$$Re \sim \frac{W V_y}{\nu} \sim \frac{W V_x}{\nu} \sim \frac{W}{\nu} \frac{F_d}{\rho U W}$$

\uparrow
y direction
(spr)
Wake flow Re

$$Re \sim F_d / \rho U W \nu$$

$$\sim U^2 R^2 \rho C_D$$

$$\sqrt{\rho} \nu (C_D R^2)^{1/3} x^{1/3}$$

$$C_D \sim 1$$

$$\sim \left(\frac{UR}{\nu} \right) \left(R/x \right)^{1/3}$$

118

$$Re(x) \sim Re_0 (R/x)^{1/3}$$

and $Re(x) \rightarrow 0$ at

$$x \sim R (Re_0)^3$$

distance behind boat where
turbulent wake transitions to
laminar.

i.e. skin l_d : transition from turbulent
mixing to viscous mixing

N.B. [In wake, vertical/rotational region
can expand into irrotational
region, but never reverse!]

i.e. would really violate H-Thm...

Later discussionWakes - SupplementSketch→ Revisit turbulent wake, using turbulent viscosity, i.e.

$$W \sim (rx/u)^{1/2} \quad (r \rightarrow \Delta_T)$$

$$\rightarrow (\Delta_T x/u)^{1/2}$$

i.e. is width of turbulent wake set by turbulent diff. following Blasius Law

but $\Delta_T \sim W \tilde{\nu} \Rightarrow$ turbulent viscosity at mixing length level.

$$\sim W (F_d / \rho u W^2)$$

$$\sim F_d / \rho u W \quad \sim \text{const} / W$$

$$\Rightarrow W \sim (F_d x / \rho u^2 W)^{1/2}$$

$$W^{3/2} \sim (F_d / \rho u^2)^{1/2} x^{1/2} \sim (C_D R^2)^{1/2} x^{1/2}$$

$$W \sim (C_D)^{1/3} R^{2/3} x^{1/3}$$

$$\sim C_D^{1/2} R x^{1/2}$$

⇒

$$w/R \sim c_D^{1/3} (x/R)^{1/3}$$

egrees ✓

Now, $D_T \sim \bar{v} w$

$$\sim \frac{(\bar{v} w^2)}{w}$$

$$\sim \frac{\rho U \bar{v} w^2}{\rho U w}$$

$$\sim \frac{Q}{w} \sim Q/R (x/R)^{1/3}$$

" - Point is that turbulent viscosity mixing drops downstream, relative to constant viscous mixing.

- follows from $\bar{v} w \sim \frac{Q}{w}$ \rightarrow const.

- explains why turbulent wake spreads more slowly than laminar wake.